

DOMAIN DECOMPOSITION TECHNIQUES FOR TREATING MULTISCALE PROPERTIES IN RESERVOIR ENGINEERING APPLICATIONS

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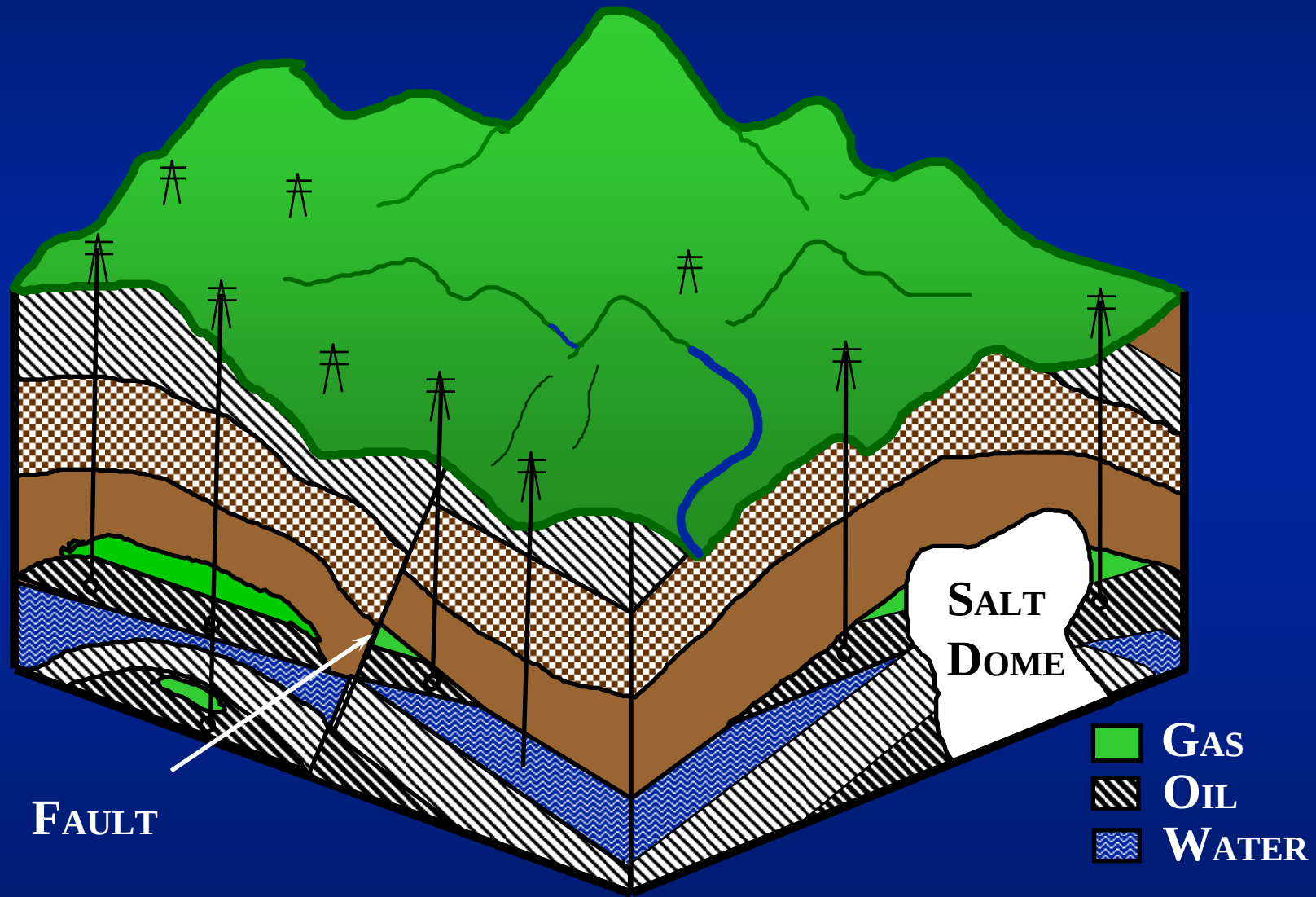


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GAS, OIL, WATER



TRANSPORT IN POROUS MEDIA

PHYSICAL RELATIONS:

CONSTITUTIVE LAW (D'ARCY)

$$\mathbf{u} = -T \nabla \Phi$$

CONSERVATION OF MASS

$$-\operatorname{div} \mathbf{u} = \frac{\partial}{\partial t} (\phi S(\Phi)) + q$$

COMPONENT BALANCES

$$\frac{\partial}{\partial t} (\phi f_1(c)) + \operatorname{div}(\mathbf{u} f_2(c)) = \nabla \cdot (D \nabla c) + q(c)$$

EQUATIONS OF STATE

THERMAL BALANCE

UPSCALING

$$\tilde{u} = -\frac{\tilde{K}}{\mu} \nabla \Phi,$$

$\tilde{K}$ = Effective Permeability

$$\frac{\partial}{\partial t}(\phi c) + \nabla \cdot (\tilde{u} c) - \nabla \cdot \tilde{D}(\tilde{u}) \nabla c = \hat{q} c, \quad \tilde{D} = \text{Macrodispersity}$$

- ◆ GELHAR, AXNESS - WATER RES. RES., 1983
- ◆ DAGAN - FLOW & TRANS. POROUS MEDIA, 1989
- ◆ EWING, RUSSELL, YOUNG - 10 SPE RES. SIM., 1989
- ◆ ESPEDAL, LANGLO, SAEVAREID, GISLEFOSS - SPE 21231, 1991
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- ◆ GLIMM, LINDQUIST, PEREIRA, ZHANG - TRANS. POROUS MEDIA, 1993
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- ◆ EFENDIEV, DURLOFSKY, LEE - WATER RES. RES., 2000
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- ◆ GINTING, EWING, EFENDIEV, LAZAROV - JCAM, 2004



SINGLE-PHASE FLOW EQUATIONS

D'ARCY'S LAW: $u = -\frac{K}{\mu}(\nabla p - \rho g \nabla z)$

MASS BALANCE: $\frac{\partial}{\partial t}(\phi \rho) + \nabla \cdot (u \rho) = q$

TRANSPORT: $\frac{\partial}{\partial t}(\phi c) + \nabla \cdot u c - \nabla \cdot D(u) \nabla c = \lambda(c) + q c$

WHERE

$$D_{ij} = \phi(x) \left[d_m I + \frac{d_\ell}{|u|} \begin{pmatrix} u_1^2 & u_1 u_2 \\ u_1 u_2 & u_2^2 \end{pmatrix} + \frac{d_t}{|u|} \begin{pmatrix} u_2^2 & -u_1 u_2 \\ -u_1 u_2 & u_1^2 \end{pmatrix} \right] \\ + \text{Nonlocal Dispersion } (t)$$

MULTI-COMPONENT MISCIBLE TRANSPORT UPSCALING

WE EXPAND ABOUT COARSE GRID VALUES OF THE C AND v

$$C = \bar{C} + C', \quad v = \bar{v} + v'$$

AND PERFORM A PERTURBATION ARGUMENT TO OBTAIN

$$\frac{\partial \bar{C}}{\partial t} + \bar{v} \cdot \nabla \bar{C} + \overline{v' \cdot \nabla C'} = 0.$$

THE TERM $\overline{v' \cdot \nabla C'}$ REPRESENTS SUBGRID EFFECTS AND CAN BE COMPUTED FROM THE EQUATION FOR FLUCTUATION

$$\frac{\partial C'}{\partial t} + v \cdot \nabla C' + v' \cdot \nabla \bar{C} - \overline{v' \cdot \nabla C'} = 0.$$

PROJECTING THIS EQUATION ONTO $dx(\tau)/d\tau = v$, WE HAVE

$$\frac{dC'}{d\tau} = -v' \cdot \nabla \bar{C} + \overline{v' \cdot \nabla C'}.$$

INTERGRATING OVER 0 TO t , WE OBTAIN THE SOLUTION OF THIS EQUATION ALONG THE TRAJECTORY

$$C'(x, t) = \int_0^t \left(-v'(x(\tau), \tau) \cdot \nabla \bar{C}(x(\tau), \tau) + \overline{v'(x(\tau), \tau) \cdot \nabla C'(x(\tau), \tau)} \right) d\tau.$$

MULTI-COMPONENT MISCIBLE TRANSPORT UPSCALING

SUBGRID EFFECTS CAN BE WRITTEN AS

$$\overline{v'_i(x,t)C'(x,t)} = -\overline{v'_i(x,t)} \int_0^t \overline{v'(x(\tau),\tau) \cdot \nabla \bar{C}(x(\tau),\tau)} d\tau.$$

THE EQUATION OBTAINED IS AN INTEGRO-DIFFERENTIAL EQUATION. IF WE ASSUME THAT THE CONCENTRATION VARIES SLOWLY ALONG STREAMLINES, THEN

$$\overline{v'_i(x,t)C'(x,t)} \approx -\sum_j \left(\int_0^t \overline{v'_i(x,t)v'_j(x(\tau),\tau)} d\tau \right) \frac{\partial \bar{C}(x,t)}{\partial x_j}.$$

THE COARSE-SCALE EQUATION IS

$$\frac{\partial \bar{C}(x,t)}{\partial t} + \bar{v} \cdot \nabla \bar{C}(x,t) - \nabla \cdot (D(x,t) \nabla \bar{C}(x,t)) = 0,$$

WHERE $D_{ij}(x,t) = \int_0^t \overline{v'_i(x,t)v'_j(x(\tau),\tau)} d\tau.$

D DEPENDS ON THE CONCENTRATION BECAUSE THE VELOCITY DEPENDS ON THE CONCENTRATION VIA FLOW EQUATIONS



MACRODISPERSION COMPUTATIONS

IF $L_j(x,t) = \int_0^t \dot{v}_j(x(\tau), \tau) d\tau$ (LENGTH OF TRAJECTORY IN j DIRECTION), THEN

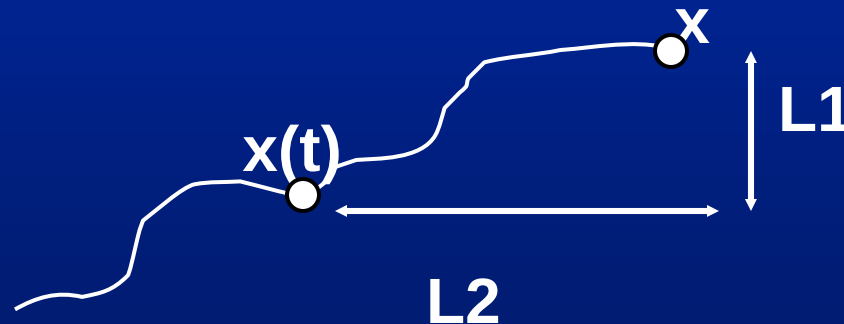
$$D_{ij}(x,t) \approx \overline{\dot{v}_i(x,t)} L_j(x,t).$$

WE CAN SHOW THAT

$$L_j(x,t) = L_j(y_p, t_p) + (t - t_p) \dot{v}_j(x,t),$$

i.e., THE MACRODISPERSION CAN BE COMPUTED LOCALLY IN TIME (WE DO NOT NEED THE HISTORY OF THE VELOCITY):

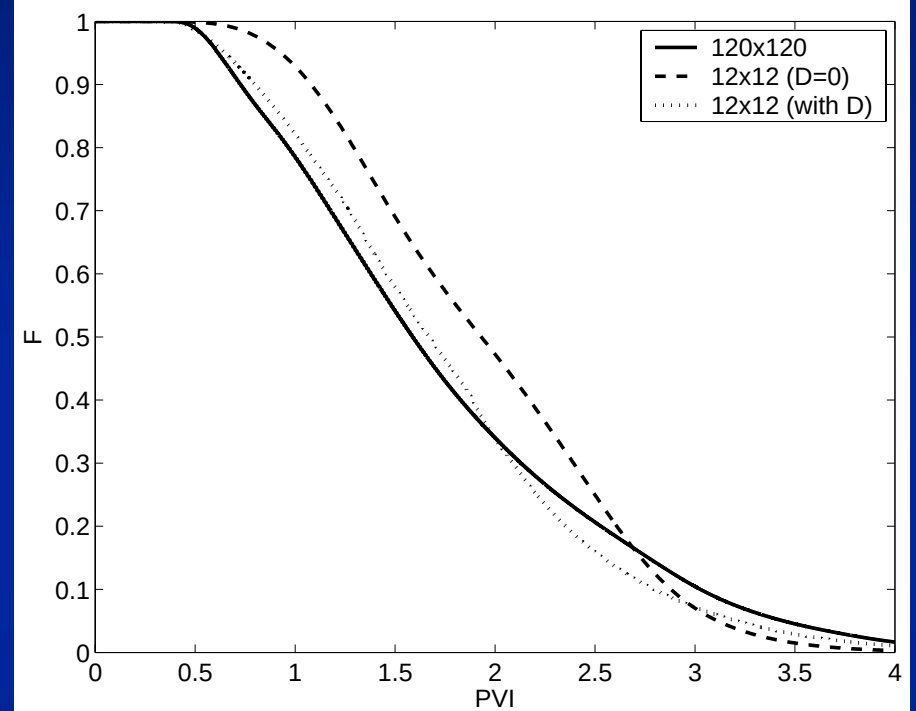
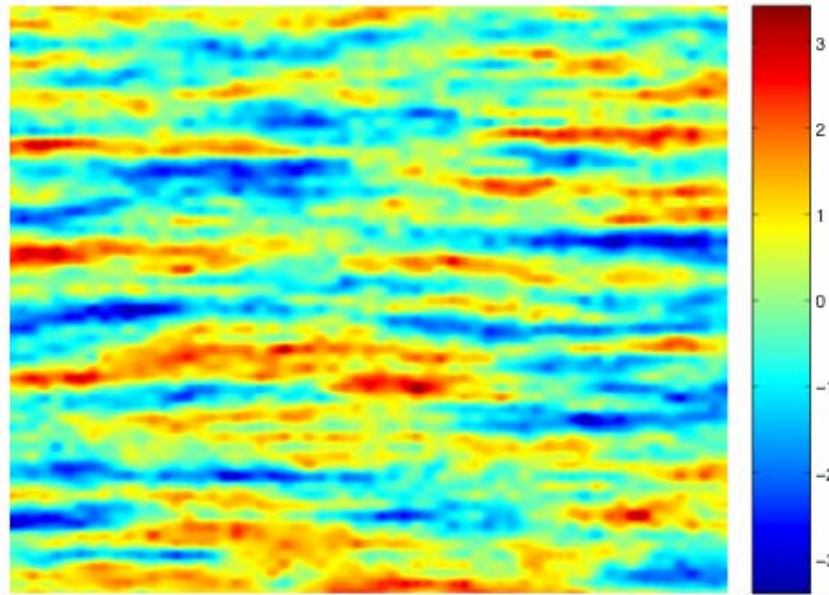
$$D_{ij}(x,t) \approx \overline{\dot{v}_i(x,t)} L_j(y_p, t_p) + (t - t_p) \overline{\dot{v}_i(x,t)} \dot{v}_j(x,t).$$



UPSCALING OF FLOW EQUATIONS

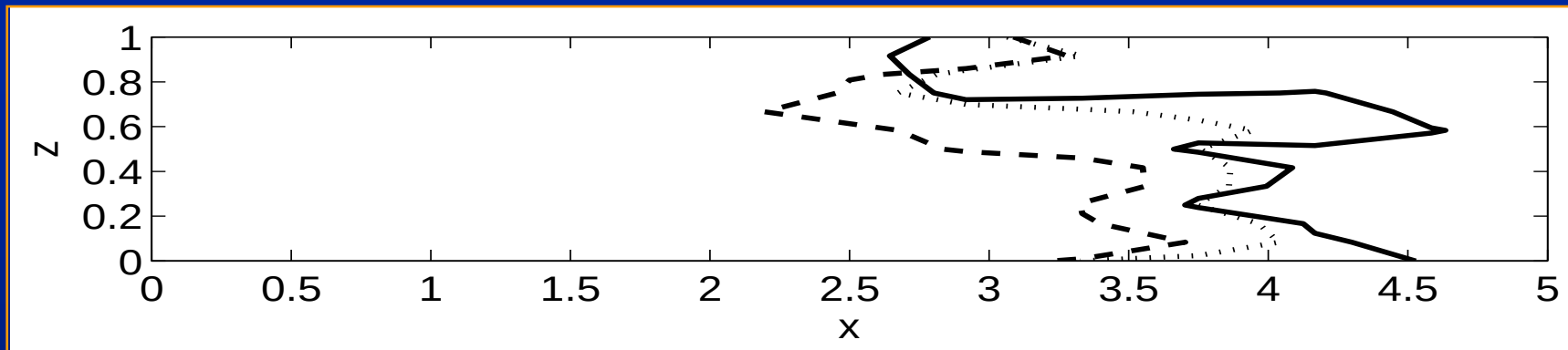
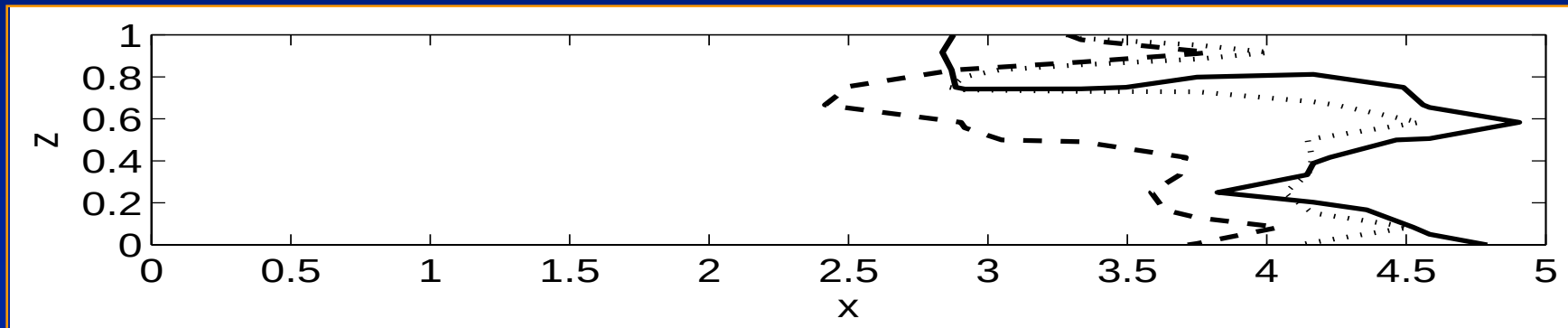
- ◆ FOR UPSCALING OF THE PRESSURE EQUATION, MULTISCALE FINITE VOLUME ELEMENT METHOD IS USED. THE IDEA OF THIS METHOD IS TO CAPTURE THE SUBGRID EFFECTS USING MULTISCALE BASIS FUNCTIONS. THIS ALLOWS US TO RECOVER SUBGRID EFFECTS OF THE VELOCITY FIELD LOCALLY AND COMPUTE THE MACRODISPERSION.
- ◆ ADAPTIVE LOCAL GRID RE FINEMENT CAN BE USED NEAR SHARP FLUID INTERFACES TO RESOLVE THE FINER SCALE AND MORE COMPLEX PHYSICS.

NUMERICAL RESULTS



$$l_x = 0.20, l_z = 0.02, \sigma = 1.5, M=2$$

NUMERICAL RESULTS



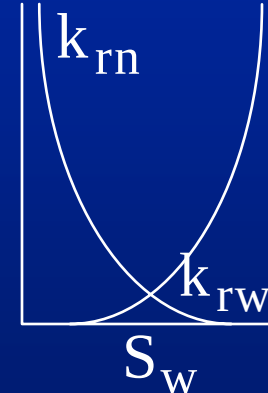
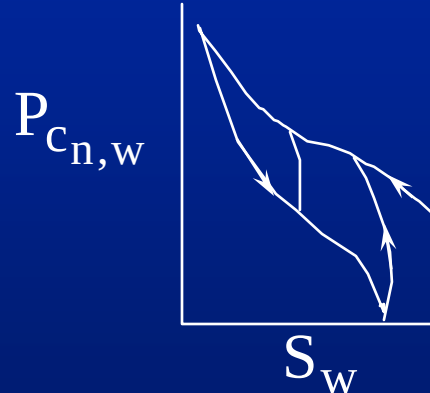
TWO-PHASE FLOW

D'ARCY'S LAW:
$$u_i = -\frac{Kk_{ri}}{\mu_i}(\nabla p_i - \rho_i g \nabla z), \quad i = w, n$$

MASS BALANCE:
$$\frac{\partial}{\partial t}(\phi \rho S_i) + \nabla \cdot (\rho_i u_i) = q_i \rho_i, \quad i = w, n$$

$$p_{c_{n,w}} = p_n - p_w, \quad S_n + S_w = 1$$

w = Wetting Phase
n = Nonwetting Phase



MULTIPHASE FLOW EQUATIONS

$$S_a c_a \frac{dp}{dt} + \nabla \bullet u + S_a c_a f_w \frac{dp_c}{dt} = -\frac{\partial \phi}{\partial t} + q_t$$

$$\phi \frac{\partial S_w}{\partial t} + \nabla \bullet f_w u + \nabla \bullet K f_a f_w \lambda (\nabla p_c - G_l) = -S_w \frac{\partial \phi}{\partial t} + q_w$$

WHERE

$$u = -K \lambda (\nabla p + G), u = u_a + u_w$$

$$p = S_a p_a + S_w p_w + \frac{1}{2} \int_0^{p_c} (f_a - f_w) d\eta$$

$$\lambda_i = k_{ri} / \mu_i, f_i = \lambda_i / \lambda, i = a, w$$

$$\frac{\partial}{\partial t} \equiv \phi \frac{\partial}{\partial t} + u_a / S_a \bullet \nabla, \lambda = \lambda_a + \lambda_w$$

COMPOSITIONAL MODEL

$$\frac{\partial}{\partial t}(n_w \phi) + \nabla \cdot \left(\frac{n_w}{V_w} \mathbf{u}_w \right) = q_w$$

$$\frac{\partial}{\partial t}(n^i \phi) + \nabla \cdot \left(\frac{n_o^i}{V_o} \mathbf{u}_o + \frac{n_g^i}{V_g} \mathbf{u}_g \right) - \nabla J^i = q^i \quad i = 1, \dots, N_C$$

$$\mathbf{u}_\alpha = \frac{K k_{r\alpha}}{\mu_\alpha} (\nabla p_\alpha - \rho_\alpha g \nabla z) \quad \alpha = o, w, g$$

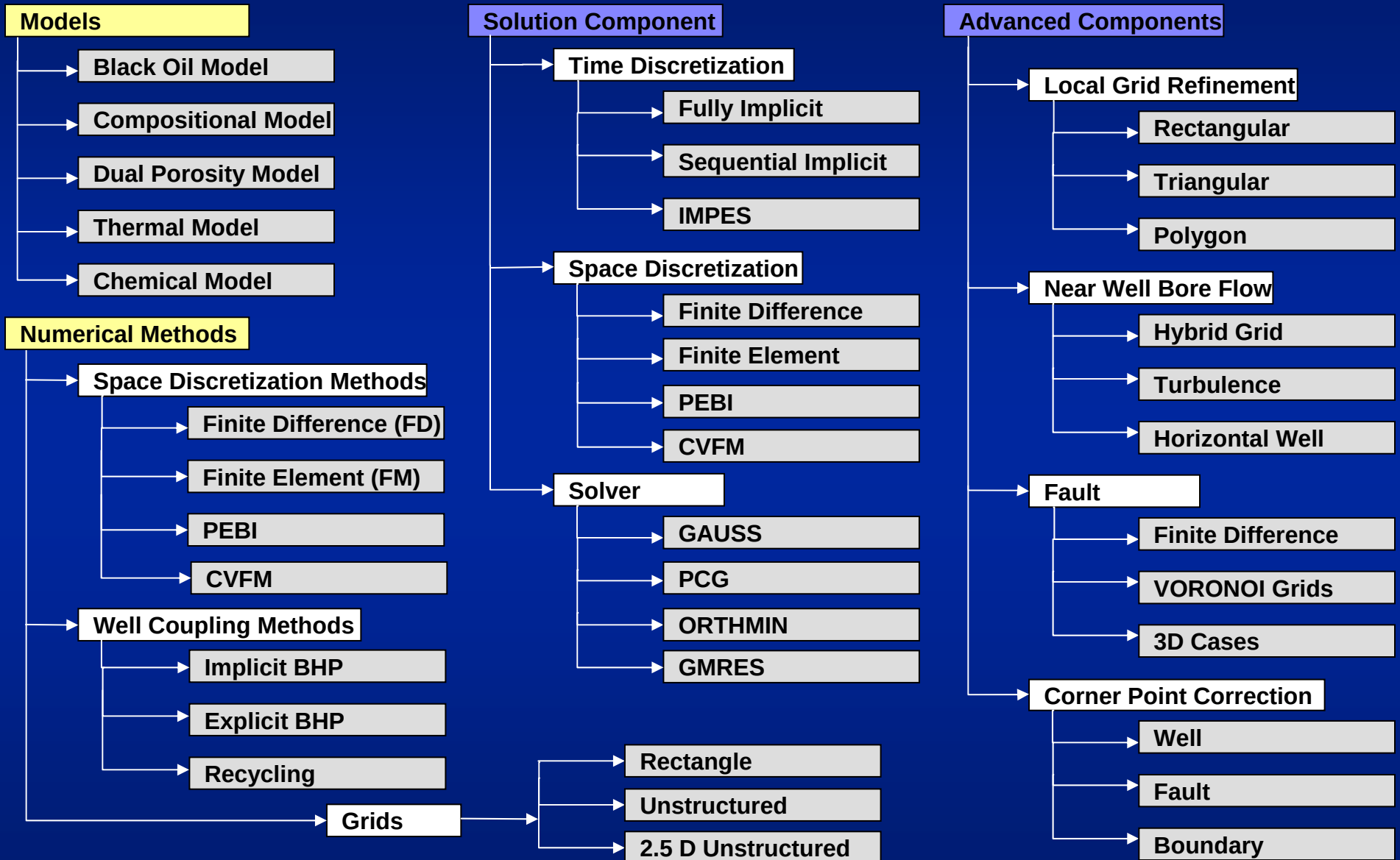
PHASE PACKAGE:

PARTITION COEFFICIENTS

CUBIC EQUATION OF STATE



APPLICATION/MODULES IN RESERVOIR SIMULATION



EXAMPLE SCENARIO IN RESERVOIR SIMULATION

Method Options

- Fully Implicit
- Sequential Implicit
- IMPES

- Finite Difference
- Finite Element
- PEBI
- CVFM

- GAUSS
- PCG
- ORTHMIN
- GMRES

Workflow

Begin

Problem Definition

Time Discretization

Space Discretization

Solver

End

Application Modules

Input

Nonlinear PDEs

Linear Algebraic Equations

Staged Output

Final Output

Control

Logic



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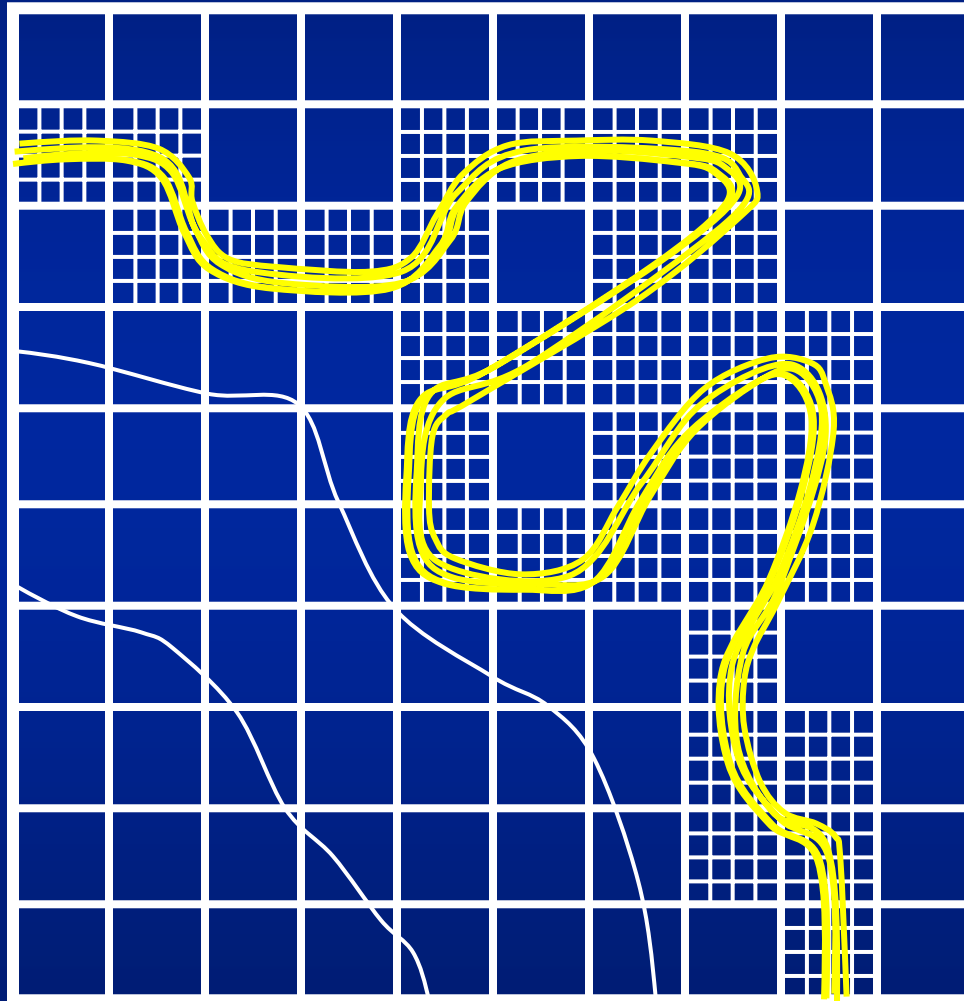
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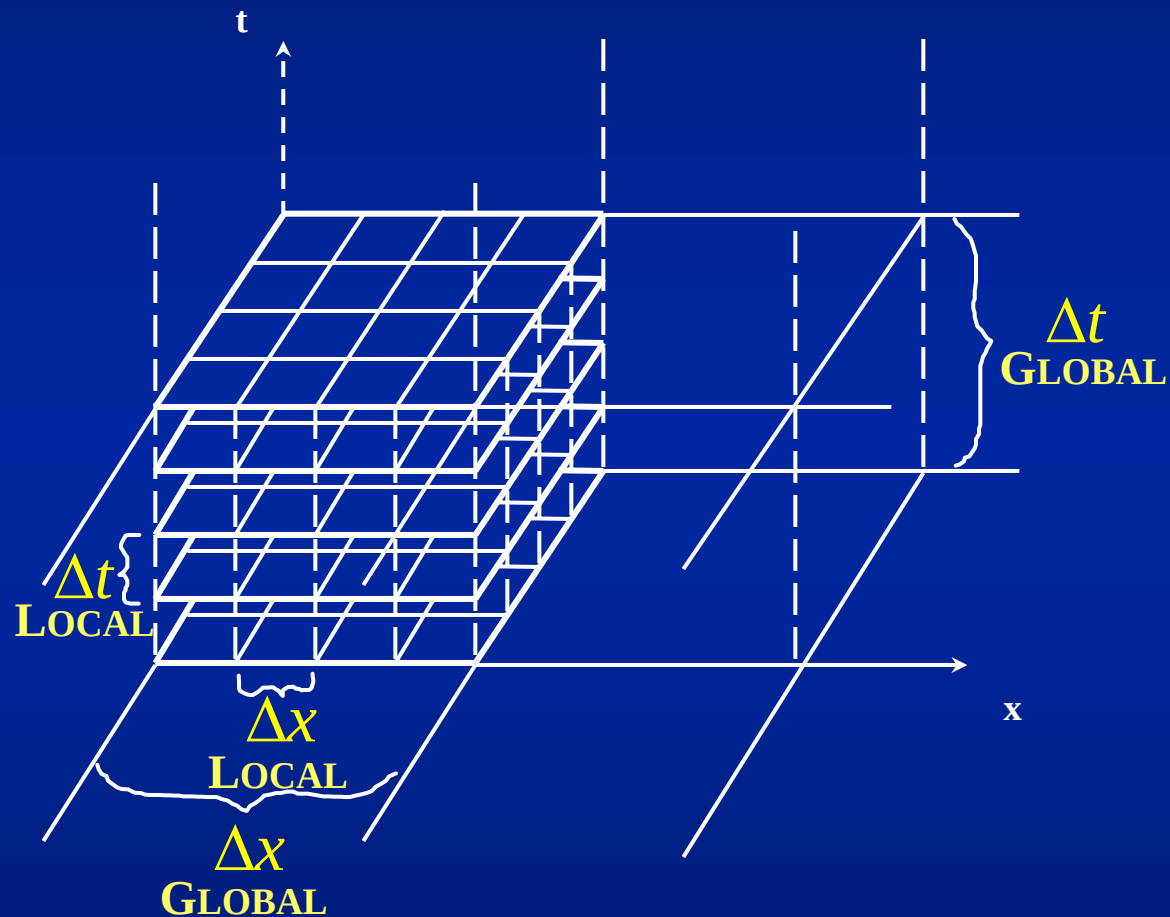


Saevareid, Espedal, *et al.* 1992.

MULTIPHASE FLOW SATURATION CONTOURS



LOCAL TIME – STEPPING



LOCAL TIME – STEPPING METHODS

EWING, LAZAROV, VASSILEVSKI – I – COMPUTING, 1990

EWING, LAZAROV, VASSILEVSKI – II – LNFS, 1990

DAWSON, DU, DUPONT – UC – 1989

DAWSON, DU, DUPONT – UC – 1989

HEROX, THOMAS – PROC. CMMG – 1989

ERIKSON, JOHNSON – UG – 1989

EWING, LAZAROV, PASCIAK, VASSILEVSKI – SINUM – 1993

EWING, JACOBS, PARASHKEVOV, SHEN – SIAM 1991

BOYETT, EL-MANDOUH, EWING – SIAM – 1991

EWING, LAZAROV, VASSILEV – CMAME – 1992

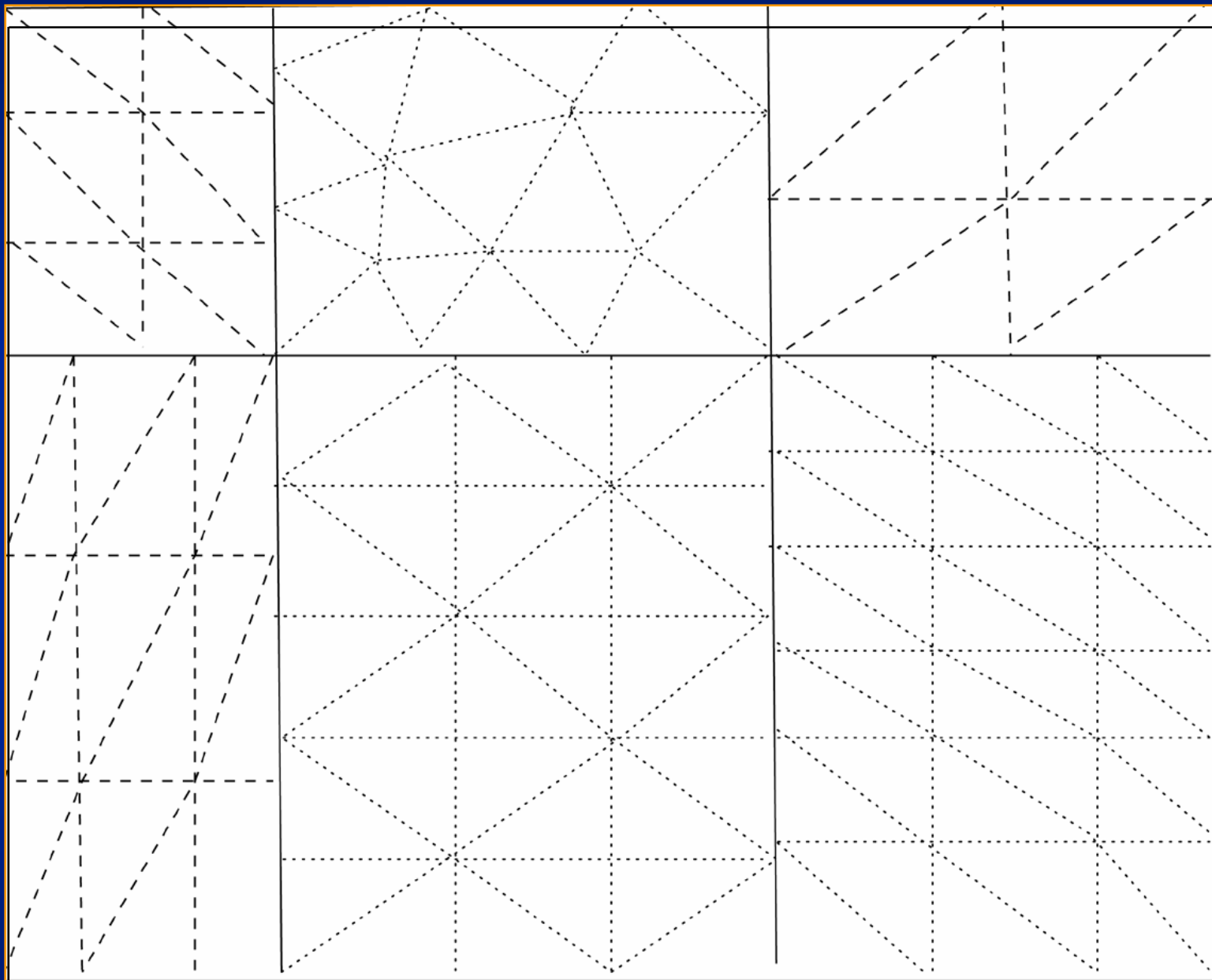
JACOBS – PH.D. THESIS – 1995

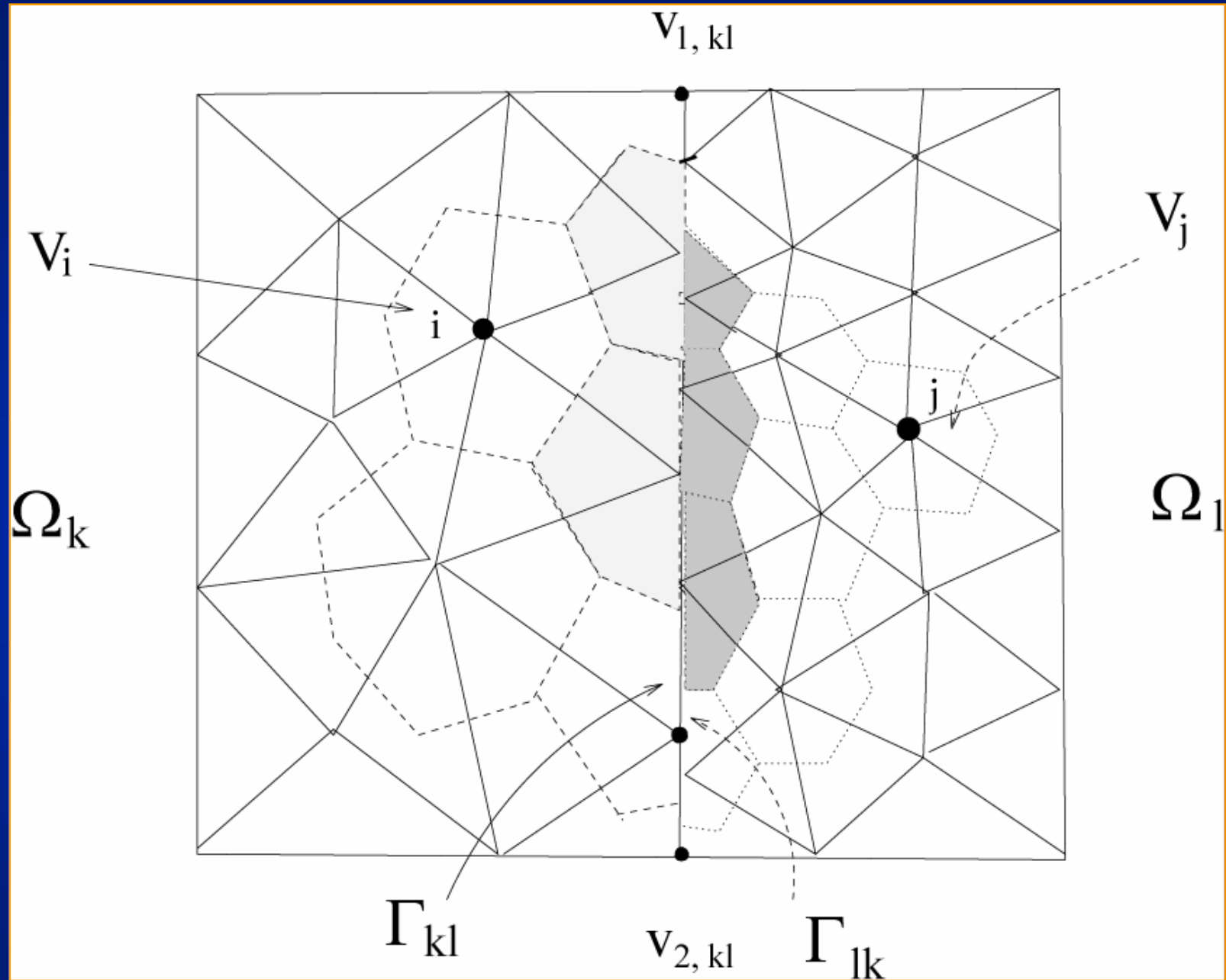
EWING, LAZAROV, VASSILEV – SINUM – 1994

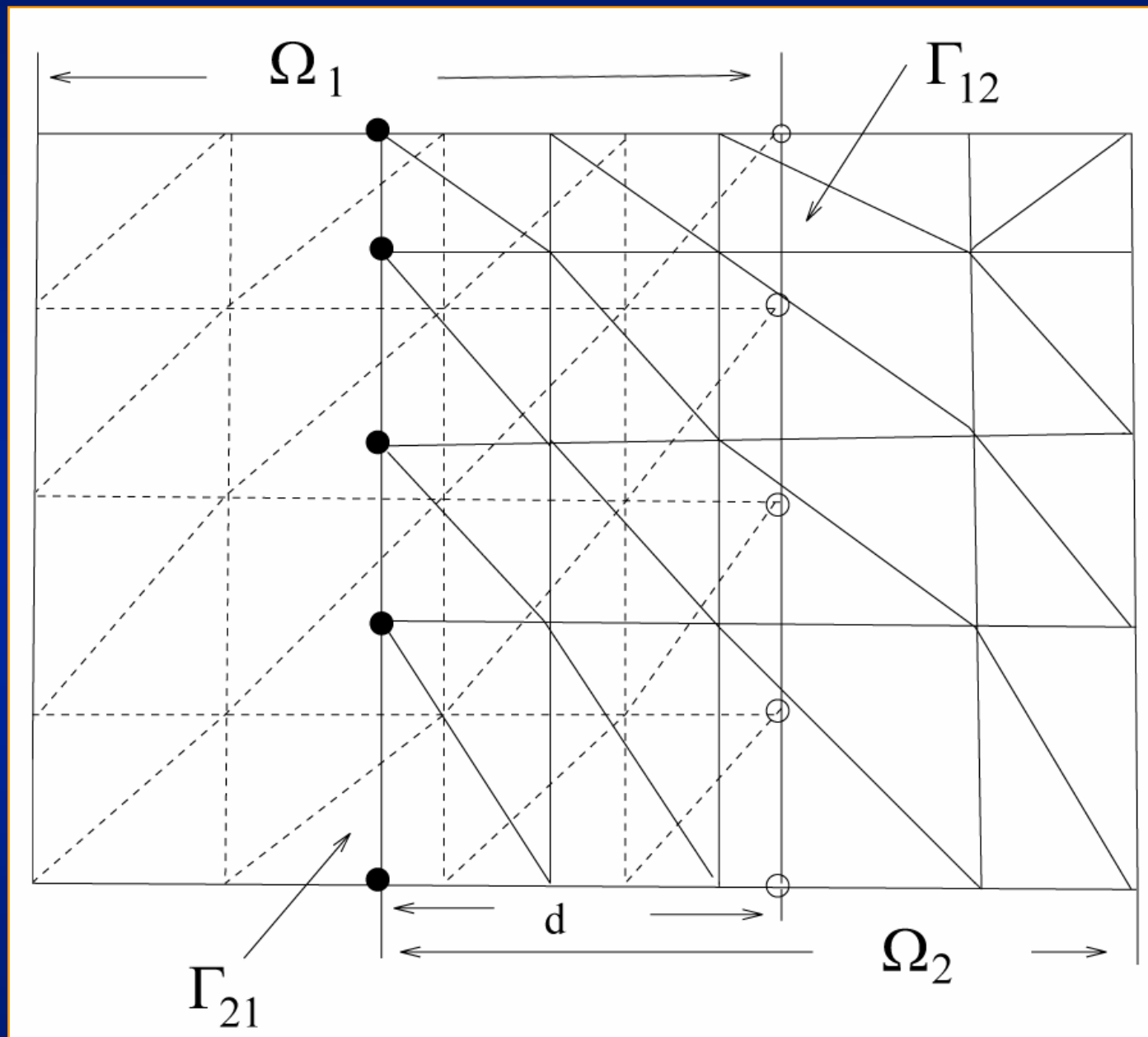
THEOREM: (E,L,V)

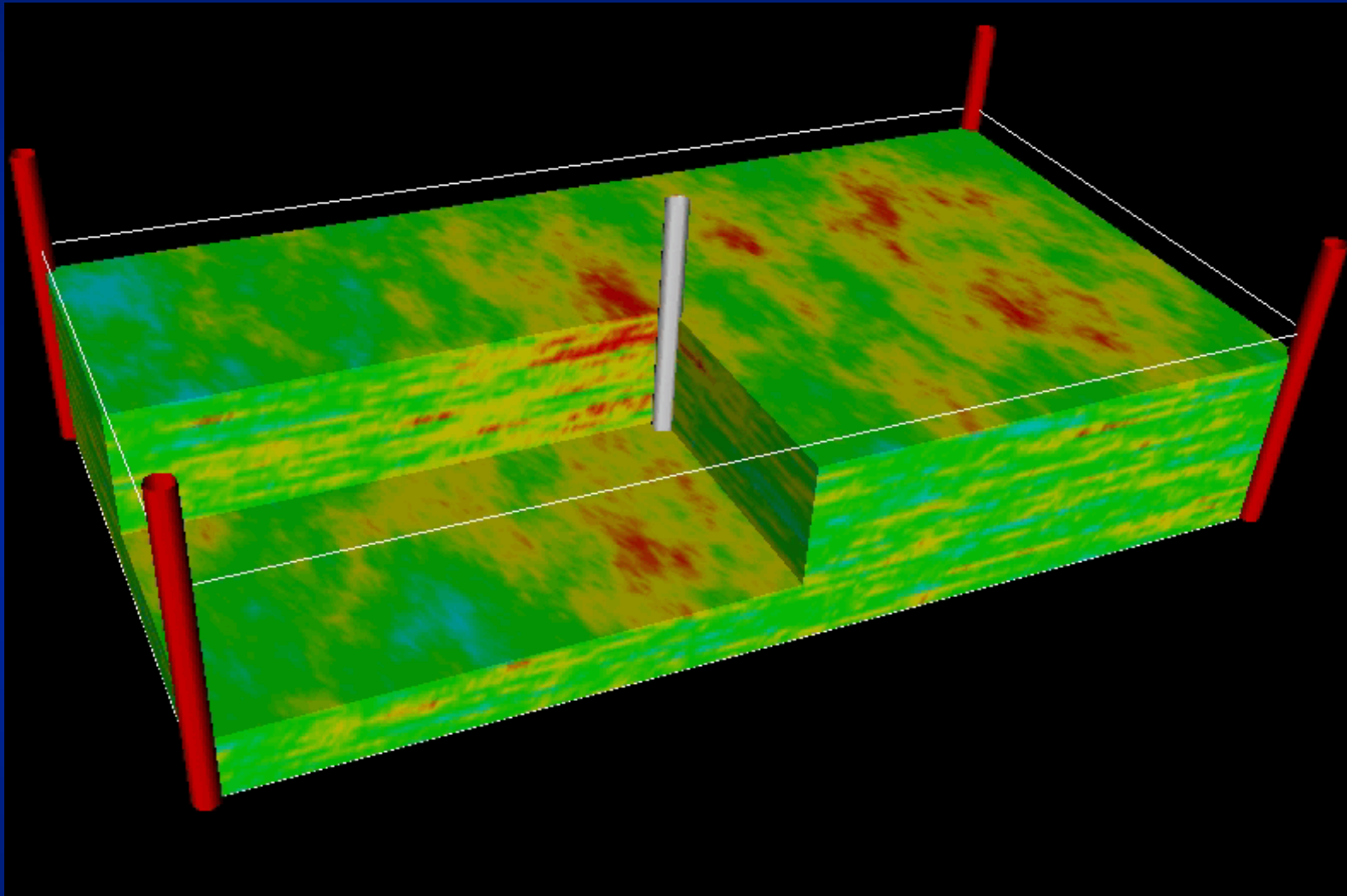
$$\max_{(x,t) \in J} |e(x,t)| \leq C_c (\tau_c + h_c^2) + C_f (\tau_f + h_f^2) + C_I \left(\tau_c + h_c^2 + \frac{\tau_c^2}{h_c} \right)$$

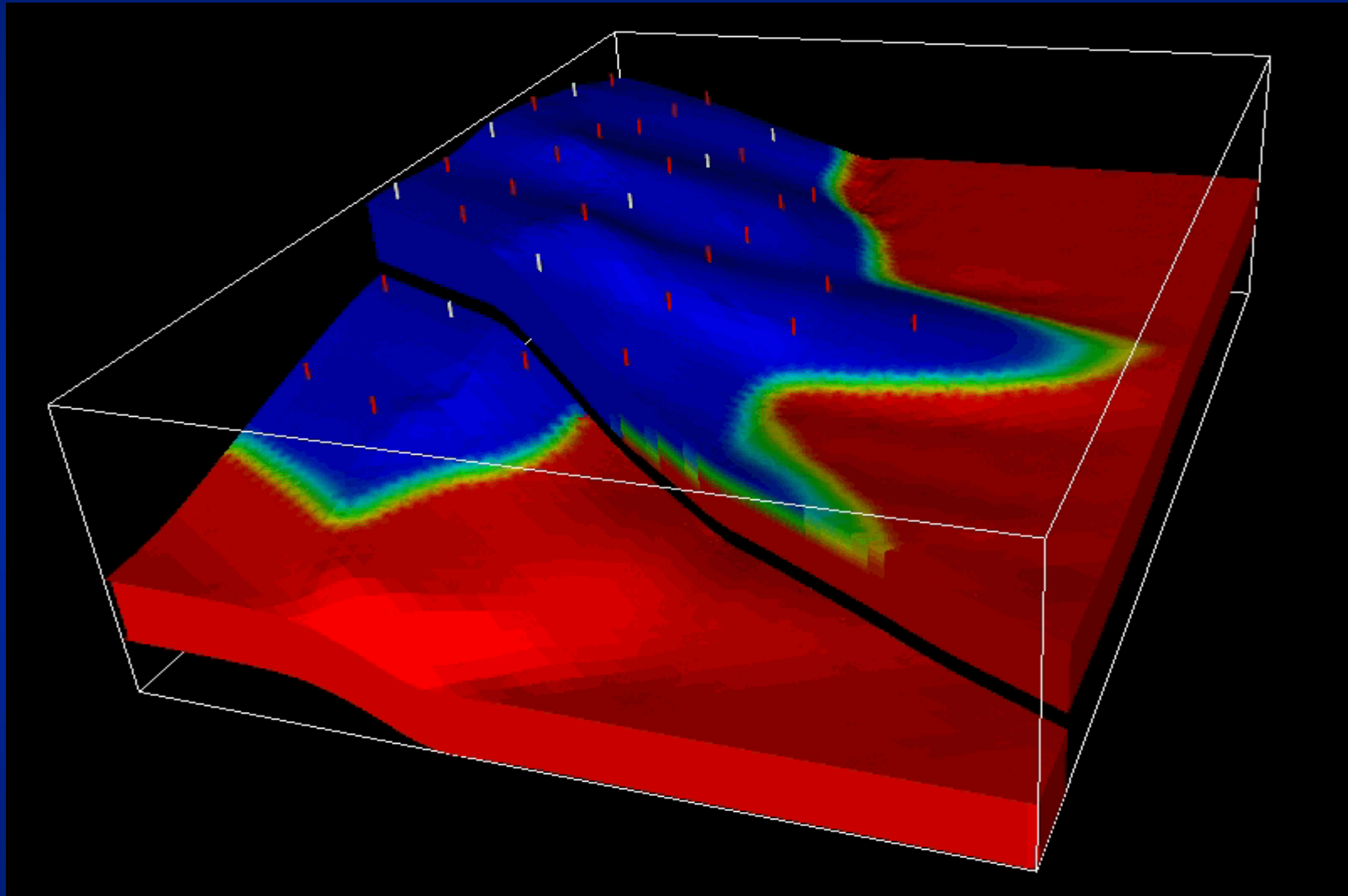












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